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Evaluation of HPCD batch treatments on enzyme inactivation kinetics and selected quality characteristics of cloudy juice from *Golden delicious* apples

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HPCD inactivation rate of PPO and PME increased with increasing p and T.

Sensitivity to temperature change is similar for HPCD and mild thermal treatment.

PME is more HPCD resistant than PPO.

HPCD treatment decreased particle size of cloudy apple juice.

Colloidal stability and nutritional properties were not affected by HPCD.

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1 **Evaluation of HPCD batch treatments on enzyme inactivation kinetics and selected**
2 **quality characteristics of cloudy juice from *Golden delicious* apples**

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7
8 **Abstract**

9 Cloudy apple juice has been treated by high pressure carbon dioxide (HPCD) as non-thermal
10 technology to inactivate polyphenoloxidase and pectinmethylesterase in batch mode. Stirring
11 speed (from 200 to 600 rpm) induced an increase in the enzyme inactivation rate while a triple
12 cycle of pressurization/depressurization led to the same enzyme inactivation efficiency. Enzyme
13 inactivation kinetics were determined at different temperatures (from 35 to 45 °C) and pressures
14 (from 10 to 20 MPa). Data were described by the first order kinetic model and the Weibull
15 model. For the first order kinetic model, decimal reduction time for HPCD treatment was found
16 to be smaller than for mild heating, in the same temperature range. The same tendency was
17 observed for the first decimal reduction time in the Weibull model. HPCD treatment resulted in a
18 homogenization effect reflected in the shifting of the particle size distribution towards smaller
19 diameters after treatment. HPCD treatment did not result in a change of water and oxalate
20 soluble pectin content, total phenolic compounds and hidroxymethylfurfural content.

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23 *Keywords:* Cloudy apple juice, HPCD, inactivation kinetics parameters, properties

24 **1. Introduction**

25 Consumption of cloudy apple juice seems to be more beneficial than consuming clear apple juice
26 due to changes in phenolic compounds and loss of pectins during clarification process
27 (Markowski et al., 2015). However, color and cloud stability are main challenges in preservation
28 of cloudy apple juice during its processing and storage. Enzymatic browning in cloudy apple
29 juice is due to the action of polyphenol oxidase (PPO) that catalyzes the oxidation of phenolic
30 compounds to quinones. On the other hand, the mechanism of cloud stability is not yet
31 understood. Among the different mechanisms proposed, electrostatic repulsion by negative
32 charges present in the partly demethylated pectin due to galacturonic residues could be
33 responsible of cloud stability avoiding aggregation (Zhao et al., 2008). In this regard, the activity
34 of pectinmethylesterase (PME) causes pectin demethylation that could precipitate with calcium
35 ions present in the juice causing clarification and the loss of turbidity. However, other
36 components with negative charge have been also reported in the literature as stabilizing agents of
37 the cloud in the serum such as phosphatide acids of cloud lipids (Krapfenbauer et al., 2006).
38 Thermal treatments have been traditionally used for the inactivation of microorganisms and
39 enzymes that affect negatively the quality of foods. However, these methods cause undesirable
40 effects in quality attributes such as flavor and loss of nutritional components. High pressure
41 carbon dioxide (HPCD) treatment has been proposed as an alternative non-thermal pasteurization
42 technique that can inactivate certain microorganisms and enzymes under mild operation
43 conditions. Typically, operating pressure does not exceed 50 MPa and temperature ranges
44 between 20 and 50 °C, below pasteurization temperature (Manzocco et al., 2016). The
45 mechanism of pressurized CO₂ on enzyme inactivation is not yet fully understood. In the

46 literature different approaches can be found such as pH lowering due to dissolved CO₂,
47 conformational changes or formation of different complex with CO₂ molecules (Hu et al., 2013).
48 Some studies have been found in the literature regarding the effect of HPCD on enzymes of
49 cloudy apple juice from *Fuji* apples. Niu et al. (2010) evaluated the quality of cloudy *Fuji* apple
50 juice processed from apple slices previously treated by HPCD. These authors found that PPO
51 could be completely inactivated at 20 MPa for 20 min and at temperature as low as 25 °C;
52 however, residual activity of 18% was still found for PME after treatment at 65 °C and 20 MPa
53 for 20 min. Gui et al. (2007) found higher values of residual activity than the work of Niu et al.
54 (2010), for PPO in HPCD-treated cloudy *Fuji* apple juice in a batch mode (40% at 30 MPa and
55 55 °C for 60 min). When using a continuous HPCD system, holding times of 10 min were
56 needed at 22 MPa and 60 °C to achieve complete inactivation of PPO but, at the same working
57 conditions, still PME residual activity of 42% was obtained (Xu et al., 2011).

58 From previous reported results, it can be clearly observed that there is a great variety in the
59 literature data on enzyme inactivation from cloudy apple. This is a main drawback in the
60 commercialization of this technology and reliable data on juice quality are still needed.

61 According to Wang et al. (2010) the influence of agitation on enzyme inactivation under high-
62 pressure environment is a key factor in the design of reactors of industrial scale volume.
63 However, the effect of stirring speed on enzyme activity has not been considered in most of the
64 studies. Wang et al. (2010) determined the effect of agitation at 40°C on isoamylase, obtained
65 from a fermentation broth from *Pseudomonas amyloclavata* after cell removal, and a
66 commercial β -amylase under supercritical carbon dioxide, at different operating times (up to 120
67 min) and different operating pressure (from 11.0 to 17.2 MPa), observing that the activity of both
68 enzymes decreased by increasing the speed of agitation.

69 In this work, the effect of HPCD treatment on some quality characteristics of cloudy apple juice
70 from *Golden delicious* has been studied. The effect of some variables, non-previously studied in
71 literature, on enzyme inactivation from cloudy apple juice, has been considered such as the effect
72 of stirring speed and the number of successive pressurization/depressurization cycles. Enzyme
73 inactivation kinetic data parameters are also necessary to scale-up HPCD process. This regard,
74 enzyme inactivation kinetics of PPO and PME have been determined at different operating
75 pressures and temperatures. Enzyme inactivation kinetic data have been described by the first
76 order kinetic model and the Weibull model as an alternative to the classical first order kinetic
77 model. Some other important quality parameters of cloudy apple juice have been also determined
78 before and right after HPCD treatment, such as pectin content, particle size distribution, color
79 and antioxidant capacity.

80 **2. Materials and methods**

81 **2.1 Juice preparation**

82 *Golden delicious* apples were peeled and cut in cubes and then added to a 0.3 % of L-ascorbic
83 acid solution to avoid enzymatic browning during processing. Apple cubes were wiped and
84 immediately squeezed with a screw juice extractor. The liqueur was filtered with 2 layers of
85 cheesecloth. The pH of the juice obtained was 3.89 ± 0.01 and the soluble solid content was 12.5
86 ± 0.1 °Brix. The juice was stored frozen at -18 °C until further use.

87 **2.2 HPCD equipment and processing**

88 The HPCD cell was made of stainless steel (SS-316) and had an internal volume of 100 mL with
89 a maximum operating pressure and temperature of 30 MPa and 80 °C, respectively (Melgosa et
90 al., 2017). For each experiment, 40 mL of apple juice were charged into the high pressure cell
91 that was immersed in a thermostatic water bath at the operating temperature. The magnetic
92 stirring was then connected and the system was pressurized by a using a syringe pump with a

93 pressure controller (ISCO 260 D) up to the desired pressure. CO₂ was fed into the high pressure
94 cell through a sintered stainless steel micro-filter with a pore size of 10 μm (Briongos et al.,
95 2016). This regard, Ishikawa et al. (1995) showed that the concentration of CO₂ in the sample
96 was influenced by the way CO₂ was fed into the sample, increasing by decreasing the pore size
97 of the filter at 25 MPa and 35°C.

98 Samples were collected periodically to follow the inactivation kinetics of the enzymes.
99 Experiments were carried out in the ranges of temperature (T) from 35 to 45 °C, pressure (p)
100 from 10 to 20 MPa and stirring speed from 200 to 600 rpm. The effect of the sampling procedure
101 and the number of pressurization/depressurization cycles on enzyme activity was also analyzed.

102 To compare the effect of the HPCD treatment on enzyme activity with mild heating treatment,
103 cloudy apple juice was heated at atmospheric pressure in the same temperature range (from 35 to
104 45 °C). Samples were taken periodically at different treatment times up to 120 min.

105 Some other important quality attributes of cloudy apple juice, such as particle size distribution, ξ
106 potential, turbidity, pH, pectin content, total phenolic compounds, non-enzymatic browning and
107 antioxidant capacity were also determined before and right after HPCD treatment.

108 **2.3 Physico-chemical analysis**

109 **2.3.1. Determination of PPO activity**

110 The activity of PPO was determined spectrophotometrically by using a 0.05 M catechol (Sigma
111 Aldrich) solution prepared in a 0.1 M phosphate buffer (pH 6.5) as substrate. Samples were
112 analyzed by adding 100 μL of apple juice into 2.9 mL substrate solution. Oxidation of catechol
113 was determined immediately by the increase in absorbance at 420 nm by using a Jasco V-750
114 spectrophotometer equipped with a Peltier thermostated cell holder and a water pump to keep the
115 temperature constant at 30 °C. The PPO activity was taken as the very first linear part of the
116 reaction curve.

117 2.3.2. Determination of PME activity

118 PME activity was determined by using an automatic titrator system (Metrohm ® Titrand) by
119 using a 1 % of pectin solution (Alfa Aesar ® pectin citrus) prepared in NaCl 0.3 M as substrate.
120 50 mL of pectin solution was mixed with 1 mL of cloudy apple juice and pH was adjusted to 7.5
121 with NaOH 0.02 N. During pectin hydrolysis at 30 °C, pH was maintained at 7.5 by adding
122 NaOH 0.02 N. The amount of NaOH added for 15 min was recorded. One PME activity unit
123 (UPE) is defined as the micromoles of carboxylic groups produced per minute and mL of juice at
124 pH 7.5 and 30 °C (Briongos et al., 2016).

125 Relative residual activities of PPO and PME were evaluated as:

$$126 \text{ Residual activity, RA} = \frac{\text{Enzyme specific activity after HPCD treatment}}{\text{Enzyme specific activity in the untreated juice}} \cdot 100\% = \frac{A}{A_0} \cdot 100 \quad [1]$$

127 2.3.3. Determination of pectic substances

128 Pectic substances in cloudy apple juice before and after HPCD treatment have been determined
129 according to Robertson (1979) by progressive extraction of the alcohol insoluble solids by water
130 (high methoxyl pectins are extracted) and ammonium oxalate (low methoxyl pectins are
131 extracted). Water soluble pectins play an important role in the turbidity of the cloudy apple
132 juices acting as colloid stabilizers, while oxalate-soluble fraction can form gels with polyvalent
133 metal ions (Robertson, 1979). Pectic substances are determined spectrophotometrically at
134 520 nm after total hydrolysis to galacturonic acids by using m-hydroxydiphenil (MHDP) as a
135 chromogenic reagent. Solutions were freshly prepared before analysis: 0.15% solution of m-
136 hydroxydiphenil (Sigma Aldrich) in 0.5% NaOH and 0.0125 M sodium tetraborate (Panreac) in
137 concentrated sulphuric acid. For pectin determination, 1 mL of water extract and 5 mL of the
138 sodium tetraborate solution were mixed and placed in a water-ice bath. The mixture is then
139 heated in water bath at 80 °C for 6 min and subsequently cooled again in a water-ice bath.

140 0.1 mL of the m-hydroxydiphenyl solution was added and after homogenization of the mixture,
141 absorbance at 520 nm was measured as a function of time. According to Ibarz et al. (Ibarz et al.,
142 2006) spectrophotometric data measurements were taken at the highest absorbance instead of at a
143 certain reaction time. A calibration curve was prepared with standard solutions of D-galacturonic
144 acid (Sigma Aldrich) by following the same colorimetric method. A blank was also prepared
145 with no D-galacturonic acid.

146 **2.3.4. Particle size distribution and zeta-potential**

147 Particle size distribution (PSD) was determined by laser diffraction with a Mastersizer 2000
148 (Malvern® Inst., MA). The system uses a laser light at 750 nm wavelength to size particles from
149 0.4 to 2000 μm by light diffraction. Particle size distribution was calculated by the Fraunhofer
150 model. Size distributions (volume fractions against particle size) before and after HPCD
151 treatment were calculated and the weight-average sizes expressed as:

152 • The equivalent surface area mean diameter: $D(3,2) = \frac{\sum n_c d_{lc}^3}{\sum n_c d_{lc}^2}$ [2]

153 • The equivalent volume mean diameter: $D(4,3) = \frac{\sum n_c d_{lc}^4}{\sum n_c d_{lc}^3}$ [3]

154 where d_{lc} is the diameter of the particle and n_c is the percentage of particles.

155 To describe distribution width one common parameter is the Span:

156
$$\text{Span} = \frac{D_{v,0.9} - D_{v,0.1}}{D_{v,0.5}}$$
 [4]

157 where $D_{v,0.9}$, $D_{v,0.1}$ and $D_{v,0.5}$ are the particle size below which, 90%, 50% and 10% of the
158 particles lies.

159 ζ -potential was determined with a Zetasizer Nano ZS apparatus, using the Laser Doppler
160 Velocimetry techniques. Samples were diluted 1:50 with deionized water and filtered through
161 5 μm filter. ζ -potential gives an indication of the potential stability of a colloidal system and it is
162 a good index of the colloidal electrostatic repulsive forces. Particles will repel each other when

163 having a large negative or positive ζ -potential. Soluble pectin carries negative charge being
164 important to keep a high ζ -potential. Particles with ζ -potentials more positive or negative than
165 30 mV or -30 mV are normally considered stable (Genovese and Lozano, 2001).

166 **2.3.5. Total phenolic compounds and antioxidant capacity**

167 Total phenolic compounds were determined by using the Folin-Ciocalteu reagent (VWR). First,
168 100 μ L of the juice were mixed with 2.8 mL of water and subsequently 100 μ L of the Folin-
169 Ciocalteu reagent, in that order. After that, 2 mL of sodium carbonate 7.5% (w/v) were added
170 and the reaction started. Color was measured after 60 min of reaction at 750 nm at 21 °C. A
171 blank was also prepared using water instead of juice. A calibration curve was prepared with
172 standard solutions of gallic acid by following the same colorimetric method.

173 Antioxidant capacity was determined by the ABTS method. The ABTS method is based on the
174 decolorization of the radical cation 2,2'-azinobis-(3-ethylbenzothiazoline-6-sulfonic acid)
175 (ABTS $^{\cdot+}$). This radical is produced by oxidation of a 7 mM solution of ABTS with potassium
176 persulfate (2.45mM), allowing the mixture to stand in the dark at room temperature for 16 h
177 before use (Re et al., 1999). The ABTS $^{\cdot+}$ solution was diluted with ethanol to reach an
178 absorbance close to 0.7 at 734 nm and equilibrated at 21 °C. Diluted ABTS $^{\cdot+}$ solutions were
179 reduced in the presence of hydrogen-donating antioxidants present in the apple juice. For the
180 antioxidant test, juice samples were diluted 1:10 with deionized water. A ratio of 100 μ L/1 mL
181 (diluted cloudy apple juice/ABTS $^{\cdot+}$ solutions) was chosen and absorbance was registered along
182 time at 734 nm, since antioxidant activity depends on the selected time point (Re et al., 1999).
183 All the spectrophotometric measurements have been carried out at 21 °C in a Jasco (V-750)
184 spectrophotometer with Peltier temperature control. Results were expressed as inhibition
185 percentage of the radical ABTS $^{\cdot+}$.

186 **2.3.6. Turbidity, pH, color and non-enzymatic browning**

187 Turbidity of cloudy apple juice was measured at room temperature by diluting it 1/20 with
188 distillate water (Xu et al., 2011). A turbidimeter (Eutech Instruments, TN-100) was used and
189 turbidity was expressed as nephelometric turbidity units (NTU). pH of apple juice was
190 determined with a pH-meter (Crison® pH & Ion-Meter GLP 22).

191 The L^* , a^* and b^* values were obtained respectively by a suitable program installed in a
192 Beckman DU-650 spectrophotometer with diode-array of UV-vis (Beckman Instruments),
193 representing brightness, red to green color and yellow to blue color, respectively. Other
194 conditions are illuminant D65 (daylight source) and a 10° standard observer (perception of a
195 human observer) following the CIE recommendations. Changes in color were expressed as:

$$\Delta E = \sqrt{(L_{\text{before}}^* - L_{\text{after}}^*)^2 + (a_{\text{before}}^* - a_{\text{after}}^*)^2 + (b_{\text{before}}^* - b_{\text{after}}^*)^2} \quad [5]$$

196 According to Krapfenbauer et al. (2006) a casual viewer can notice a difference between two
197 colors when ΔE is higher than 2-3.5, although they pointed out that a trained eye is capable of
198 differentiating two colors that differ by $\Delta E < 2$.

199 Non enzymatic browning reactions are important parameters that determine the quality of food
200 products during processing and storage. Non enzymatic browning in the juice is measured as
201 hydroxymethylfurfural (HMF) concentration. 0.7 mL of juice was mixed with 0.7 mL of ethanol
202 in a 1.5 mL Eppendorf tube. The mixture was centrifuged at 12000 g for 10 min. After that,
203 1 mL of the supernatant is mixed with 1 mL of a trichloroacetic acid solution (734 mM) and
204 1 mL of a thiobarbituric acid solution (25 mM) in a closed recipient. Samples were incubated at
205 40 °C during 50 min in an agitated batch and absorbance was measure at 443 nm. A blank was
206 also prepared with distilled water instead of juice. A calibration curve was prepared using
207 different concentrations of HMF from 0.5 mg/L to 10 mg/L.

208 2.4 Kinetic data analysis

209 The knowledge of the kinetic parameters that describe the time course of the enzyme inactivation
 210 is of great importance for a correct design of a HPCD process. Gui et al. (2007) obtained good
 211 results by fitting the inactivation kinetics of PPO in cloudy apple juice to a linear kinetic model.
 212 In this work, the inactivation kinetic data at different operating temperatures and pressures were
 213 described by using two different models: (1) a first-order kinetic model, and (2) the Weibull
 214 model.

215 The first-order kinetic model can be described as:

$$216 \log \frac{A}{A_0} = -kt \quad [6]$$

217 where A_0 is the initial activity of the enzyme, A is the residual activity at different treatment
 218 times, k is the inactivation rate constant at the operating conditions (min^{-1}) and t is the treatment
 219 time (min).

220 z_T and z_P (temperature and pressure increase needed for a 90% reduction of the D value,
 221 respectively) were evaluated as the negative reciprocal slope of the regression line of $\log D$ as
 222 function of T or p respectively:

$$\log \left[\frac{D_1}{D_2} \right] = \frac{T_2 - T_1}{z_T} \quad [7]$$

$$\log \left[\frac{D_1}{D_2} \right] = \frac{p_2 - p_1}{z_P} \quad [8]$$

223 The dependence of the inactivation rate constant on temperature and pressure can be expressed
 224 through the Arrhenius and Eyring equations respectively:

$$225 \ln \left[\frac{k_1}{k_2} \right] = \frac{E_a}{RT} \left[\frac{1}{T_2} - \frac{1}{T_1} \right] \quad [9]$$

$$226 \ln \left[\frac{k_1}{k_2} \right] = \frac{V_a}{RT} [p_2 - p_1] \quad [10]$$

227 where p_2 , p_1 , T_2 , T_1 are pressures and temperatures corresponding to the decimal reduction times
 228 D_1 and D_2 or constant k_1 and k_2 , respectively, R is the universal gas constant, E_a , the activation
 229 energy (kJ/mol) and V_a , cm³/mol, is the activation volume.

230 The non-linear Weibull model can be written in the power-law form (Van Boekel, 2002):

$$231 \quad \log \frac{A}{A_0} = -\frac{1}{2.303} \left(\frac{t}{\alpha} \right)^\beta \quad [11]$$

232 where α is the scale parameter (a characteristic time) and β is the shape parameter. When $n < 1$
 233 indicates upward concavity and $n > 1$ downward concavity of the enzyme inactivation curve. The
 234 time required to achieve a number of decimal reductions, d , can be calculated by using the shape
 235 and scale parameters (Van Boekel, 2002):

$$236 \quad t_d = \alpha \left(-\ln(10^{-d}) \right)^{\frac{1}{\beta}} \quad [12]$$

237 **2.5 Statistical analysis**

238 Statistical analyses were conducted using software Statgraphics X64. The results are presented as
 239 a mean \pm standard deviation of at least three replicates. The significance of the differences was
 240 determined based on an analysis of the variance with the Fisher's least significant method at p-
 241 value ≤ 0.05 .

242 To estimate the kinetic parameters for the different models essayed in this work, non-linear
 243 regression was performed by using the Marquardt algorithm (Statgraphics X64). The mean
 244 relative deviation (MRD) between experimental and calculated residual activities (RA) was also
 245 evaluated:

$$\text{MRD} = \frac{1}{n} \left(\sum_{\text{all samples}} \left| \frac{\text{RA}_{\text{calc}} - \text{RA}_{\text{exp}}}{\text{RA}_{\text{exp}}} \right| \right) \cdot 100 \quad [13]$$

246

247 3. Results and discussion

248 3.1 Agitation speed

249 The effect of agitation on the inactivation of PPO from cloudy apple juice has been evaluated at
250 20 MPa and 45 °C, at three stirring speeds, 200, 400 and 600 rpm (Figure 1a). When working at
251 higher stirring speeds, the magnetic system of agitation did not work properly in our
252 experimental equipment; therefore stirring speeds higher than 600 rpm were not included in this
253 work. At any of the stirring speeds, the inactivation degree increased with increasing time. From
254 Figure 1a, it can be also observed that an increase in the stirring speed led to a higher
255 inactivation degree. Agitation speed enhanced mass transfer rate of CO₂ in the medium,
256 facilitating CO₂ solubilization and therefore the contact between CO₂ and the enzyme (Garcia-
257 Gonzalez et al., 2009). In this regard, Wang et al. (2010) also pointed out that an increase in the
258 agitation speed can create a larger amount of bubbles that help to enzyme inactivation. These
259 authors deduced an expression for enzyme inactivation as a function of N·t (stirred speed·time)
260 considering an equilibrium reaction between the native and the denatured enzyme and the
261 consequently irreversible aggregation between the denatured enzymes:

$$(A_0/A)=1+cte(N \cdot t) \quad [14]$$

262 By plotting the inverse of the residual enzyme activity versus N·t a straight line should be
263 obtained with the intercept equal to 1. Figure 1.b shows that for PPO inactivation in cloudy apple
264 juice, the ratio (A₀/A) is proportional to N·t for operation times shorter than 60 min:

$$265 (A_0/A)=1 + 1.704 \cdot 10^{-4} (N \cdot t) (R^2 = 0.940). \quad [15]$$

266 At longer treatment times, residual activities for all the three stirring speeds became nearly equal
267 and were not included.

268 3.2 Sampling procedure and number of pressurization/depressurization cycles

269 PPO activity after HPCD treatment was compared when sample was obtained after system
270 depressurization or removed while the system was under pressure for a single cycle
271 pressurization. HPCD treatment was carried out at 45 °C and 20 MPa for 15 min. No significant
272 differences have been determined among sample RA means of different sampling procedure
273 when applying the Fisher's least significant method at p-value ≤ 0.05 , with PPO RA values of 38
274 $\pm 4\%$ and $33 \pm 4\%$ when sampling was withdrawn while the system was under pressure or after
275 total depressurization, respectively.

276 The effect of a single cycle has been compared with a triple cycle for a total treatment time of
277 15 min, that is 5 min of pressure-treatment each cycle, respectively ($t_{\text{total, treatment}} = t_{\text{per cycle}} \cdot \times$
278 number of cycles). The same effectiveness for PPO inactivation was determined when applying
279 the Fisher's least significant method at p-value ≤ 0.05 , with values of $38 \pm 4\%$ and $33 \pm 3\%$ for
280 one single cycle and a triple cycle for a total treatment time of 15 min, respectively.

281 Primo et al. (2007) studied the effect of successive cycles of pressurization/depressurization in
282 HPCD treatment on inactivation of PPO from mate tea leaves extracts. They observed that PPO
283 presented a continuous loss of activity with the number of cycles at 7.05 MPa, 30 °C and 1 h
284 each cycle. However, to distinguish between the effect of the number of
285 pressurization/depressurization cycles and treatment time, comparison should be have done at
286 the same pressure and temperature conditions but for a total treatment time equal to $t_{\text{per cycle}} \cdot \times$
287 number of cycles, since time plays also an important role in batch enzyme inactivation. In any
288 case, as pointed out by Hu et al (2013) , the effect of pressurization/depressurization on the
289 activity of enzymes depends on the type of enzyme, its environment, pressure, temperature and
290 exposure time, being difficult to establish any rule. No other studies have been found in the

291 literature about the effect of the number of cycles on enzyme inactivation by HPCD on fresh
292 juices.

293 3.3 Effect of mild heating on PPO inactivation

294 PPO inactivation kinetics were determined at atmospheric pressure in the temperature range
295 from 35 to 45 °C (same temperature range as for HPCD treatment, Figure 2). The maximum
296 reduction of PPO activity was nearly 40 % after 2 h of heating at 45 °C indicating that PPO of
297 cloudy *Golden delicious* apple juice was rather stable under mild temperatures. Similar
298 inactivation degrees of PPO from cloudy *Fuji* apple juice were obtained by Gui et al. (2007).
299 After 1 hour of mild heating, these authors reached a maximum reduction of PPO activity of
300 20% at 45 °C. However, Niu et al. (2010) found that when subjecting apple slices to mild heating
301 treatment from 25 to 45 °C for 20 min and then processing them into cloudy apple juice, PPO
302 activity increased by 22-51%. Buckow et al. (2009) also found that at 45 °C, PPO activity from
303 cloudy apple juice increased 30%, attributing this behavior to the release of latent PPO.

304 Enzyme inactivation kinetic data under mild heating conditions and at atmospheric pressure were
305 described by the first-order model. Parameters are collected in Table 1. Inactivation rate
306 constant, k , increased with the operating temperature, therefore the corresponding D values
307 decreased with temperature. The temperature sensitivity parameter, z_T , and the activation energy
308 were evaluated as 36 °C and 53 kJ/mol, respectively (see Table 1). Values of the same order
309 were reported by Gui et al. (2007) for cloudy *Fuji* apple juice, 27.0 °C for z_T and 72.0 kJ/mol, for
310 E_a . Thermal stability of extracted apple PPO from *Golden delicious* was studied in the
311 temperature range from 68 to 78 °C by Yemencigly et al. (1997). These authors reported a z_T
312 value of 9.9 °C. The higher value obtained in this work for z_T in the temperature range from 35 to
313 45 °C might indicate a lower susceptibility to temperature change at temperatures lower than the

314 one observed at pasteurization temperatures. In any case, the values of the activation energy
315 were similar in both temperature ranges.

316 **3.4. Effect of HPCD treatment on PPO inactivation**

317 Enzyme inactivation kinetics for PPO of cloudy *Golden deliciuos* apple juice have been
318 determined at 10 MPa in the temperature range from 35 to 45 °C (Figure 3a). By increasing
319 temperature, enzyme inactivation rate also increased. In addition to the intrinsic effect of
320 temperature on enzyme inactivation, by increasing temperature, although CO₂ density decreased,
321 the diffusivity of CO₂ can be improved and accelerate the molecular collisions between CO₂
322 molecules and the enzyme. Figure 3b shows the inactivation kinetics at 45 °C in the pressure
323 range from 10 to 20 MPa. Higher operating pressures led to faster inactivation rates, but the
324 fraction of the resistant form of the enzyme was nearly independent of the operating pressure,
325 being around 6 %. This value was lower than the minimal residual activity of PPO from cloudy
326 *Fuji* apple juice reported by Gui et al. (2007), 37%, at 30 MPa and 55 °C for 60 min. In any case,
327 comparison with other HPCD systems is difficult to establish since the inactivation reached
328 would depend not only on the type and source of the enzyme and the experimental conditions
329 such as pressure, temperature and treatment time but also on the agitation of the system and the
330 ratio sample volume/cell volume since this last parameter determines the amount of CO₂ injected
331 to the system. Unfortunately in most of the studies these parameters are not detailed. PPO from
332 cloudy *Fuji* apple juice was completely inactivated by a continuous HPCD system at 22 MPa and
333 60 °C for 10 min (Xu et al., 2011). This could suggest a higher efficiency of a continuous system
334 due to the turbulent energy, comparable with a good agitation in a discontinuous system.
335 However, 60 °C cannot be considered as non-thermal and residual activity as high as 47% was
336 obtained in the continuous system at 43 °C and 25 MPa for 2 min. (Xu et al., 2011).

337 Inactivation kinetic data by HPCD were fitted to the first order kinetic model and the Weibull
338 model (Table 2). Although the Weibull model yielded the best fitting quality, the first order
339 kinetic model described the inactivation curve quite well and therefore, kinetic parameters for
340 the linear regression model have been also listed in Table 2 for comparison with data reported in
341 the literature.

342 For the first order kinetic model, inactivation rate constant, k , increased with temperature and
343 pressure. Consequently, D values decreased with increasing pressure and temperature. At each
344 operating temperature, D values were smaller for HPCD treatment (Table 2) than the
345 corresponding values for mild heating treatment (Table 1) proving that HPCD treatment was
346 more effective than thermal treatment alone. For example D was equal to 515 min at 45 °C and
347 atmospheric pressure and decreased to 104 min at 45 °C and 10 MPa.

348 z_T and activation energy values were determined as 29 °C and 64 kJ/mol, respectively, for the
349 first order kinetic model (see Table 2). z_T and activation energy values were of the same order as
350 those listed for mild heating treatment (Table 1). This meant that the sensitivity to temperature
351 change was similar for HPCD as for mild heating treatment in the temperature range covered in
352 this work. The same tendency in z_T and E_a was found by Liu et al. (2008) in the inactivation of
353 PPO of red beet extracts. These authors found that under mild heating treatment at atmospheric
354 pressure (35-55 °C), z_T and E_a were equal to 34 °C and 57 kJ/mol, respectively. After HPCD
355 treatment at 37.5 MPa, in the same temperature range, they obtained values of 36 °C and
356 54 kJ/mol for z_T and E_a , respectively. However, Gui et al. (2007) found for PPO of cloudy *Fuji*
357 apple juice that z_T increased from 27 to 108 °C and activation energy decreased from 72 to
358 18 kJ/mol under mild heating treatment (35-55 °C) and HPCD at 30 MPa in the same
359 temperature range, respectively. This increase in z_T and decrease in E_a found by Gui et al. (2007)
360 would indicate that the enzyme inactivation become less temperature dependent under

361 pressurized CO₂. This behavior is difficult to understand and it has not been observed in our
362 work. As it has been previously mentioned, in addition to the intrinsic effect of temperature on
363 enzyme inactivation, temperature has two different effects on important properties of CO₂. An
364 increase in temperature involves an improvement of mass transport properties enhancing CO₂
365 diffusivity and the number of collisions between the CO₂ and the enzyme, but on the other hand,
366 CO₂ density and therefore CO₂ solubility in the aqueous medium decreases. It seems that these
367 effects play both an important role, since similar sensitivity to temperature was found in mild
368 heat treatment and in HPCD.

369 By using equations 8 and 10 z_p and V_a have been determined as 25 MPa and -251 cm³/mol,
370 respectively for the first order kinetic model. The negative value of the activation volume
371 indicated that PPO inactivation was favored by increasing operating pressure. Other values of
372 activation volumes reported in the literature for PPO inactivation from different sources are of
373 the same order, -271.7 and -307.9 cm³/mol for the labile and stable fraction of PPO of water
374 melon at 50 °C in the pressure range of 8-30 MPa (Liu et al., 2013) or -94.31 cm³/mol for PPO
375 from cloudy *Fuji* apple juice at 55°C in the pressure range from 8 to 30 MPa (Gui et al., 2007).

376 The Weibull parameters are also listed in Table 2. Scale, α , and shape, β , parameters were used
377 to calculate the time require to inactivate 1 log ($t_{d=1}$) of PPO. Similar to the D-values for the first
378 order kinetic model, $t_{d=1}$ decreased with operating pressure and temperature. As suggested by van
379 Boekel (2002) is important to determine the effect of temperature, and in the present work of
380 pressure, on both parameters of the Weibull model. Scale parameter was statistically significant
381 dependent on temperature and pressure, when tested at the 95% significance level for a linear
382 relationship, decreasing with pressure and temperature. The shape factor, n , was less than 1
383 except for 10 MPa and 35 °C. The concavity shape of the inactivation curve could be understood
384 as a faster inactivation of the labile form of the enzyme and the presence of a resistant form of

385 the enzyme to HPCD treatment (Figures 3a and 3b). The shape parameter, β , was found to be
386 statistically significant dependent on pressure but although there seemed to be a trend in
387 temperature dependence of β , it was not statistically significant, when tested at the 95%
388 significance level for a linear relationship. In any case, it must be highlighted that only three
389 temperatures have been studied to determine the effect of temperature. According to van Boekel
390 (2002), the scale parameter, α , could be modelled in a similar way to the classical D value of the
391 first order kinetic model, suggesting a linear dependence of the $\log \alpha$ on temperature and
392 considering that β did not depend on temperature:

$$393 \log \alpha = a_1 - b_1 T \quad [16]$$

394 A z_T' value can be also defined:

$$395 z_T' = \frac{1}{b_1} \quad [17]$$

396 The value of the z_T' is listed in Table 2, together with the quality of the fitting. Although the
397 concept of z_T and z_T' is different since z_T is obtained from the linear part, whereas z_T' takes also
398 into account the nonlinear part (Van Boekel, 2002), similar values were obtained for both
399 parameters ($z_T = 29$ °C and $z_T' = 27$ °C).

400 In this work, it was also found a linear dependence of the $\log \alpha$ on pressure:

$$401 \log \alpha = a_2 - b_2 p \quad [18]$$

402 Although it was found a statistically significant linear relationship between β and p , the inverse
403 of the slope of $\log \alpha$ versus p was also evaluated. Analogous to z_T' it was defined a z_p'

$$404 z_p' = -\frac{1}{b_2} \quad [19]$$

405 This value is reported in Table 2 and quite similar values can be observed for z_p and z_p' .

406 3.5. Effect of HPCD on PME

407 To compare the HPCD resistance of PME and PPO, PME inactivation kinetics were determined
408 for the experiments performed at 45 °C and 10 MPa and 20 MPa (Figure 4). PME inactivation
409 rate was also determined at atmospheric pressure and 45 °C. At atmospheric pressure, it was
410 found that residual PME activity was still 90% after 120 min at 45°C (Figure 4). Teleszko et al.
411 (2016) studied thermal treatment of different apple cultivars, founding that PME from cloudy
412 *Golden delicious* apple juice was one of the apple cultivars that presented strongest
413 thermostability (30% of residual activity after heating 5 min at 100 °C). Niu et al. (2010) found
414 that the RA of PME from cloudy *Fuji* apple juice from apple slices previously preheated for
415 20 min at the corresponding working temperature, varied between 82 to 72 % at 35 and 45°C,
416 respectively, but with error bars higher than 10% of RA at each temperature (graphical lecture).
417 After HPCD treatment, higher inactivation rates were observed than for mild heating treatment at
418 the same temperature. Although, residual activity was still around 60 % at 20 MPa and 45 °C
419 after 60 min. This indicates that PME from cloudy *Golden delicious* apple juice is rather stable to
420 HPCD at operating temperatures considered as non-thermal treatment. Different HPCD
421 inactivation values of PME from cloudy apple juice have been reported in the literature. Niu et
422 al. (2010) reported a minimal residual activity of 18% for PME of cloudy *Fuji* apple juice from
423 apple slices treated by HPCD at 20 MPa and 65 °C for 20 min. In a continuous system, PME
424 from cloudy *Fuji* apple juice still presented a residual activity of 40% at 22 MPa and 60°C for 10
425 min (Xu et al., 2011). HPCD inactivation of PME extracts from apple juice was found to be
426 more effectively inactivated at 30 MPa for 60 min, reaching 5% of residual activity at 55 °C (Zhi
427 et al., 2008). However, in this case, results are different to compare since an extracted enzyme
428 suspended in a buffer solution can give different inactivation results from those obtained in an
429 original juice.

430 Results obtained in this work, indicate that PME from cloudy apple juice was more resistant to
431 HPCD than PPO in the pressure range covered in this work. In the literature, as for thermal
432 treatment, the higher stability has been attributed to the more complex structure of PPO with
433 three or four subunits, in higher plants, than PME, with one subunit. This structure, makes it
434 more susceptible to HPCD treatment (Niu et al., 2010). In addition, PME in fruit juices is more
435 difficult to be effectively inactivated, since PME is bound to the plant cell wall, which contains
436 natural stabilizing factors (Zhou et al., 2010).

437 PME inactivation kinetic data were described by the first order model at atmospheric pressure
438 (Table 1). The decimal reduction time at 45 °C and atmospheric pressure was found to be much
439 higher than for PPO at the same conditions. HPCD inactivation data at 45°C and 10 MPa and
440 20 MPa were fitted to the first order kinetic model and the Weibull model (Table 2). The
441 Weibull model yielded the best fitting quality, but still an acceptable good fitting for the first
442 order kinetic model was obtained. For the first order model, inactivation rate constant increased
443 with pressure, but lower values than for PPO inactivation were obtained and therefore higher D
444 values. Regarding the Weibull model, the scale and shape parameters, both, decreased with
445 operating pressure at 45°C. These parameters were used to calculate the time needed to inactivate
446 1 log ($t_{d=1}$) of PME at the two pressures studied. The $t_{d=1}$ calculated by the Weibull model is
447 much higher than the corresponding D values by the first order kinetic model. Therefore, in this
448 case, the use of the first order kinetic model could lead to an underprocessing estimation for
449 PME inactivation.

450 **3.6. Effect of HPCD on different quality parameters of cloudy apple juice**

451 Some quality parameters have been determined right after HPCD treatment at 45 °C, 20 MPa and
452 60 min of treatment time.

453 **pH.** Initial pH of cloudy apple juice was 3.89 ± 0.01 and immediately after HPCD treatment, pH
454 dropped 0.15 units to 3.74 ± 0.01 . Significant differences have been determined among sample
455 pH averages before and after HPCD treatment when applying the Fisher's least significant
456 method at p-value ≤ 0.05 (Table 3). Gui et al (2007) reported a drop of 0.3 units from 3.95 to
457 3.66 ± 0.03 for *Fuji* cloudy apple juice after HPCD treatment at 22 MPa and 55 °C for 60 min.
458 According to Meysammi et al. (1992), juices and beverages can be considered as an aqueous
459 electrolyte system of multiple ions. Under pressurized CO₂ a number of dissociation reactions
460 can take place liberating some of them H⁺ ions that could reduce the pH of the media. In any
461 case, after 2 h after depressurization pH returned to a value close to its initial value (pH = $3.87 \pm$
462 0.01).

463 **Colour parameters.** Table 3 lists the L*, a*, b* parameters of cloudy apple juice before and
464 after HPCD treatment. During browning, the L* values decrease, the juice's colour becomes
465 darker, while a* and b* values increase, with more red and yellow components (Krapfenbauer et
466 al., 2006). After HPCD treatment, lightness (L*) presented slightly, but significant, lower values;
467 however, 99% of the lightness was still retained. No significant difference was observed in the
468 redness component but a significant increase of the yellowness (b*) value has been observed
469 indicating more yellow components right after HPCD treatment. The change in colour, ΔE (Eq.
470 5) is also presented in Table 3. Slightly noticeable differences in color after HPCD treatment
471 have been determined, $\Delta E \approx 0.51 \pm 0.05$ (Yuk et al., 2014). Other authors found that L*, a* and
472 b* values remained almost constant after HPCD treatment at 55 °C and different operating
473 pressures (8-30 MPa) for 60 min (Gui et al., 2006).

474 **Total polyphenolic compounds.** Total polyphenols remained unchanged after HPCD. Gasperi
475 et al. (2009) also found no significant differences in polyphenols content after HPCD treatment
476 of a blend of *Golden delicious* and *Granny Smith* apple at 10 MPa and 36 °C for 10 min.

477 **Antioxidant capacity.** Antioxidant capacity of Golden cloudy apple juice has been determined
478 by the ABTS tests (Table 3). Slightly higher values were obtained after HPCD treatment
479 although differences before and after treatment were found to be no significant ($p \leq 0.05$).

480 **Hydroxymethylfurfural.** Table 3 presents the HMF content before and after HPCD treatment.
481 From these results, it can be concluded that non enzymatic browning reactions were not
482 significant during HPCD processing, probably due to the mild temperatures employed in HPCD
483 treatments.

484 **Particle size distribution.** The particle size distribution of untreated cloudy apple juice ranged
485 from 0.275 μm to 416.87 μm with three maxima at 0.63, 19.96 and 208.93 μm (see Figure 5).
486 After HPCD treatment, the particle range shifted to smaller particle sizes from 0.04 μm to
487 104.71 μm with one main maximum at 0.182 μm . Table 3 lists values of D[3,2] and D[4,3] of
488 freshly cloudy apple juice and after HPCD treatment. The values after HPCD treatment were
489 significantly lower than those of freshly cloudy apple juice. The homogenization effect of HPCD
490 can be also observed in the values of d(0.1), d(0.5) and d(0.9), which correspond to the size of
491 particle below which 10%, 50% and 90% of the sample lies, respectively. This homogenization
492 effect induced by HPCD could be attributed to the explosive action and the bubbling of CO_2
493 from the juice during decompression (Zhou et al., 2010).

494 For freshly cloudy apple juice, the total volume of all particles with diameter less than 5 μm
495 represented 56.5% of the total particles volume, while this number increased up to 96% after

496 HPCD treatment. This fact is also reflected in the Span values (Table 3) that shows a higher
497 degree of uniformity of the cloudy apple juice after HPCD treatment.

498 **Turbidity.** The turbidity of the cloudy apple juice after HPCD is considerably higher than that of
499 freshly cloudy apple juice (Table 3). It seems that there was a correlation between juice's
500 turbidity and particle size distribution. However, no correlation was found with PME residual
501 activity since, after HPCD treatment, PME activity was still more than 60%.

502 **Pectin content.** In this work, soluble pectin presented slightly higher values after HPCD (Table
503 4). HPCD treatment could result in a more dissolution of pectin in fruit cell into the juice,
504 increasing the value of soluble pectin. In addition, according to the PSD previously reported,
505 HPCD induced an homogenization with lower particle size diameters, which could result in a
506 higher solubility of the pectin; since, in the literature, it has been reported that pectin solubility in
507 water increases by decreasing its polymer size (Sila et al., 2009) however no significant
508 differences have been found at $p \leq 0.05$. No significant differences have been also determined
509 for the oxalate-soluble pectin.

510 In the literature, Zhou et al. (2010) reported no change in water soluble pectin when treating
511 peach juice by HPCD at 30 MPa and 55 °C at different treatment times, although these authors
512 observed an increase of the large particle after HPCD treatment. However, Yu et al (2013)
513 observed that soluble pectin of HPCD-treated banana pulp at 20 MPa, during 30 min at different
514 temperatures in the range from 45 to 60 °C, was significantly lower than the untreated pulp.
515 These authors attributed this behavior due to interaction of pectin and protein or gelling of pectin
516 that may occur during HPCD treatment (Yu et al., 2013).

517 **ξ potential.** ξ potential is an indication of colloidal stability of the juice. Both, untreated and
518 treated apple juice presented negative values of -22.0 mV and -22.3 mV, respectively. These
519 values were within the range reported by Corak and Corredig (2006) of ξ potential as a function

520 of pH for orange juice. Negative values of ξ -potential indicated that juice particles were
521 negatively charged. The extent of this negative surface charge before and after HPCD treatment
522 involves electrostatic charge repulsion which has been established as one of the mechanisms of
523 cloud stabilization (Corak and Corredig, 2006). Since no significant differences at p-values \leq
524 0.05 were found before and after treatment, it indicates that colloid stability is kept after HPCD
525 treatment.

526 **Conclusions**

527 HPCD treatment is a valid alternative technology to process *Golden delicious* cloudy apple juice
528 being more effective than mild thermal treatment in the same temperature range.

529 PPO and PME inactivation rate increased with operating pressure and temperature, although
530 PME was found to be more HPCD resistant compared to PPO. The non linear Weibull
531 performed a better fitting of the enzyme inactivation kinetics by HPCD than the classical first
532 order kinetic model.

533 However, further research is needed to have reliable data on HPCD as cold pasteurization
534 method, since different results are found in the literature for the same fruit variety. Important
535 variables in enzyme inactivation are usually not described in the research articles such as the way
536 the CO₂ is fed into the sample, agitation speed or the ratio juice/volume of the cell that in fact
537 determined the ratio juice/CO₂. In this work, it was observed that the stirring speed was an
538 important factor to take into account for enzyme inactivation, due to an improvement in CO₂
539 diffusivity

540 HPCD induced a homogenization effect on cloudy apple juice since particle size distribution was
541 shifted to smaller particle size. Colloidal stability is not affected by HPCD treatment as well as the
542 pectic content substances. Slightly noticeable differences in color after HPCD treatment have

543 been determined ($\Delta E \approx 0.5 \pm 0.1$). Other quality parameters in cloudy apple juice, such total
544 polyphenolic compounds, antioxidant capacity or hydroxymethylfurfural content did not change
545 after HPCD treatment. Other important aspects need also to be addressed for an industrial
546 application such as sensory quality, shelf life studies and economic aspects.

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552

553 LITERATURE

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656

657 Table 1. Kinetic parameters at 0.1 MPa for the first order kinetic model for PPO inactivation by
 658 mild thermal heating (35-45°C) and PME at 45 °C.

PPO T, °C	First order kinetic model			
	k, min ⁻¹	D, min	R ²	MRD
35	0.00102 ± 0.00003	980	0.9814	1.6
40	0.00166 ± 0.00005	602	0.9791	1.1
45	0.00194 ± 0.00003	515	0.9993	1.1

z _T = 36 ± 11 °C (R ² = 0.9188)				
E _a = 53 ± 14 kJ/mol (R ² = 0.9248)				
PME, 45°C	0.00038 ± 0.00003	2632	0.9799	0.8

659 Table 2. Kinetic parameters for the Weibull and the first order kinetic models for PPO and PME inactivation by HPCD.

PPO		Weibull model					First order kinetic model			
p, MPa	T, °C	α , min	β	$t_{d=1}$, min	R^2	MRD	k, min ⁻¹	D, min	R^2	MRD
10	35	98 ± 2	1.13 ± 0.06	205	0.9940	2.3	0.0044 ± 0.0001	227	0.9891	3.4
10	40	72 ± 2	0.93 ± 0.04	177	0.9939	3.4	0.0060 ± 0.0001	167	0.992	3.9
10	45	41 ± 2	0.89 ± 0.05	105	0.9960	4.9	0.0096 ± 0.0002	104	0.992	6.8
z' _T = 27 ± 4 °C; (R ² = 0.9726)							z _T = 29 ± 3 °C; (R ² = 0.9897)			
							E _a = 64 ± 8 kJ/mol; (R ² = 0.9834)			
12.5	45	30 ± 1	0.74 ± 0.02	93	0.9983	2.9	0.015 ± 0.001	67	0.966	23.6
15	45	23.7 ± 0.4	0.70 ± 0.02	78	0.9995	1.2	0.019 ± 0.001	53	0.953	15.6
20	45	17.2 ± 0.9	0.59 ± 0.02	71	0.9981	5.9	0.026 ± 0.004	38	0.965	44.3
z' _P = 27 ± 3 MPa; (R ² = 0.9729)							z _P = 25 ± 5 MPa; (R ² = 0.9226)			
							V _a = -251 ± 48 cm ³ /mol; (R ² = 0.9332)			
PME		α , min	β	$t_{d=1}$, min	R^2	MRD	k, min ⁻¹	D, min	R^2	MRD
p, MPa	T, °C									
10	45	785 ± 294	0.55 ± 0.09	3576	0.9587	2.3	0.0015 ± 0.0001	667	0.9424	5.2
20	45	373 ± 74	0.45 ± 0.04	2380	0.9940	1.1	0.0037 ± 0.0006	270	0.9181	8.6

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662

663 Table 3. Some quality parameters before and right after HPCD treatment of cloudy apple juice at
 664 20 MPa and 45 °C after 60 min.

Parameter	Before HPCD	After HPCD
pH	3.89 ± 0.006 ^a	3.74 ± 0.006 ^b
Color $\Delta E = 0.51 \pm 0.05$	L* = 37.30 ± 0.03 ^a a* = 1.6 ± 0.1 ^a b* = 7.90 ± 0.03 ^a	L* = 36.98 ± 0.01 ^b a* = 1.59 ± 0.08 ^a b* = 8.26 ± 0.07 ^b
Total polyphenols, mg galic/L	456.1 ± 13.1 ^a	455.4 ± 4.3 ^a
ABTS, % of inhibition	20 min, 49 ± 2 ^a 60 min, 65 ± 2 ^a 120 min, 81 ± 3 ^a	20 min, 52 ± 3 ^a 60 min, 68 ± 4 ^a 120 min, 85 ± 4 ^a
Non-enzymatic browning, (mg HMF/L)	2 ± 0.3 ^a	1.70 ± 0.09 ^a
PSD	D(3,2) = 1.7 ± 0.07 μm^a D(4,3) = 109 ± 3 μm^a d(0,1) = 0.59 ± 0.01 μm^a d(0,5) = 13 ± 1 μm^a d(0,9) = 337 ± 7 μm^a Span = 26 ± 7 μm^a	D(3,2) = 0.21 ± 0.01 μm^b D(4,3) = 2.4 ± 0.2 μm^b d(0,1) = 0.099 ± 0.001 μm^b d(0,5) = 0.265 ± 0.006 μm^b d(0,9) = 1.63 ± 0.07 μm^b Span = 5.8 ± 0.1 μm^b
Turbidity, NTU	105 ± 2 ^a	168 ± 3 ^b
Water soluble pectin	22 ± 2 ^a	28 ± 3 ^a
Oxalate soluble pectin (mg galacturonic/L)	23 ± 4 ^a	23 ± 3 ^a
ζ -potential	-22.0 ± 0.3 ^a	-22.3 ± 0.4 ^a

665 Values with different letters in **each row** (a, b) are significantly different when applying the Fisher's least significant
 666 method at p-value ≤ 0.05 .

667

668 **List of Figure captions**

669 **Figure 1. (a)** Effect of stirring speed on PPO inactivation from cloudy apple juice by HPCD at
670 20 MPa and 45 °C (\diamond 200 rpm, Δ 400 rpm, \circ 600 rpm). **(b)** Inverse of residual activity of PPO
671 versus the product of number of revolutions per time and treatment time ($N \cdot t$) at 20 MPa and 45
672 °C (stirring speed range: 200 to 600 rpm). The continuous line corresponds to the linear fitting
673 (Eq. 15).

674 **Figure 2.** Inactivation of PPO in cloudy apple juice at atmospheric pressure at different mild
675 temperatures (35 °C \diamond , 40 °C \circ , 45 °C \square). The continuous lines represent the first order model
676 (Table 1).

677 **Figure 3.** Inactivation of PPO in cloudy apple juice by HPCD **(a)** 10 MPa and different
678 temperatures (35 °C \diamond , 40 °C \circ , 45 °C \square) **(b)** 45°C and different pressures (10 MPa \square , 12.5 MPa
679 Δ , 15 MPa \diamond , 20 MPa \circ). The continuous lines represent the Weibull model (Table 2).

680 **Figure 4.** Inactivation of PME in cloudy apple juice under mild heating treatment at 45°C (Δ
681 atmospheric pressure) and by HPCD at 45 °C (10 MPa \square , 20 MPa \circ). The continuous lines at
682 atmospheric pressure represent the first order kinetic model (Table 1), while in HPCD treatment
683 represent the Weibull model (Table 2).

684 **Figure 5.** Particle Size Distribution (PSD) of cloudy apple juice before treatment (—) and after
685 HPCD treatment at 45 °C, 20 MPa for 60 min (-·-·-).

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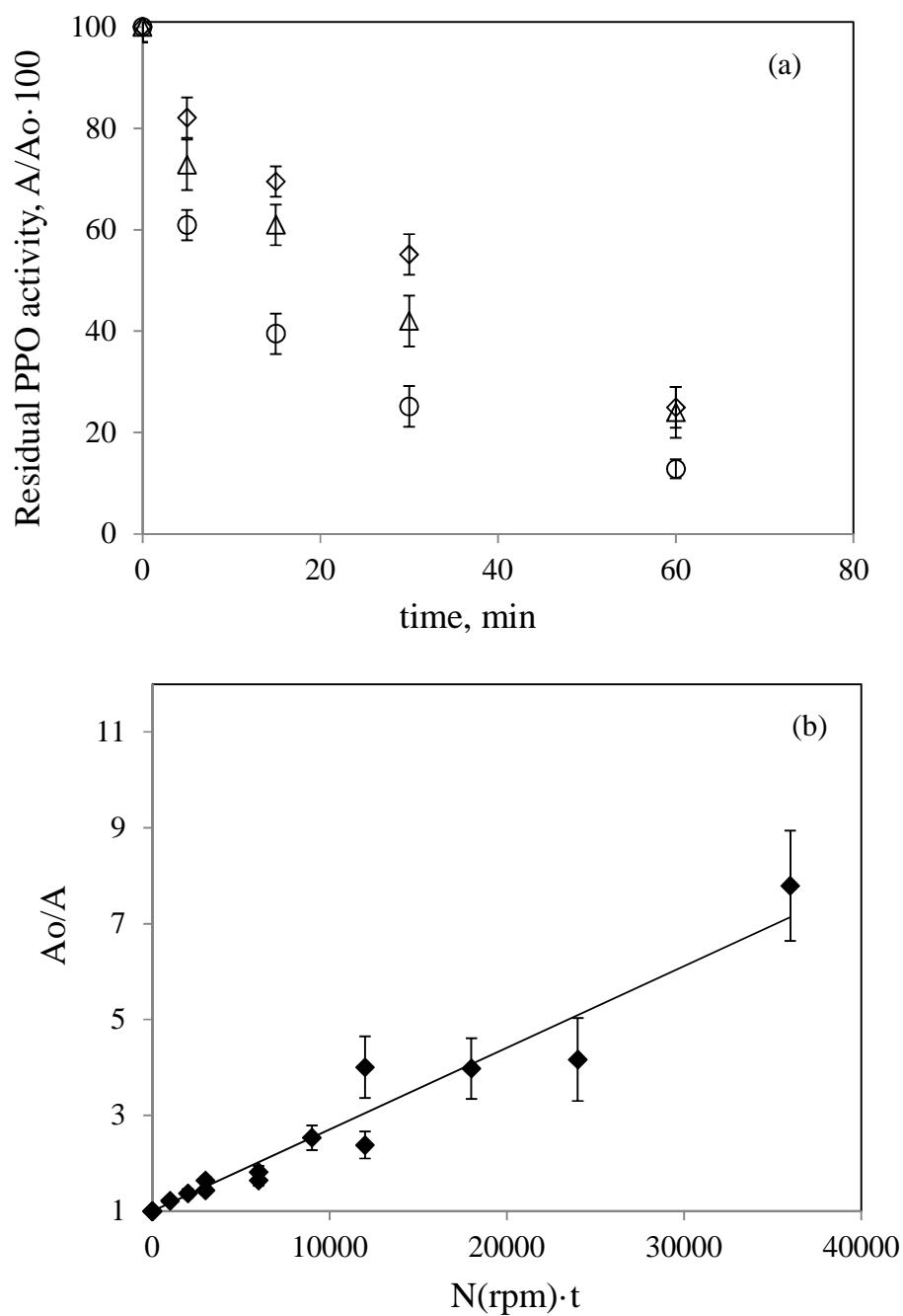
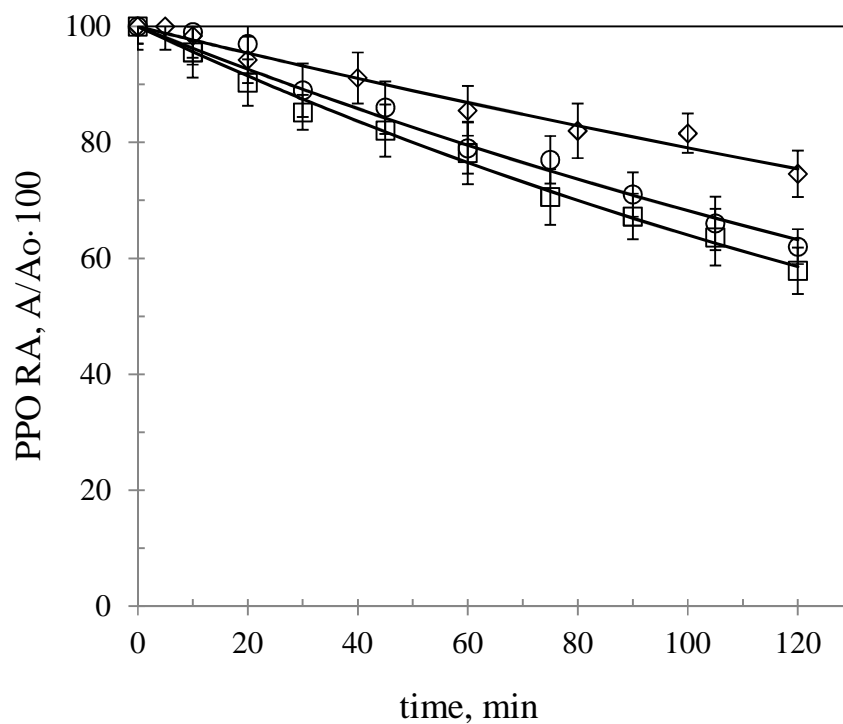


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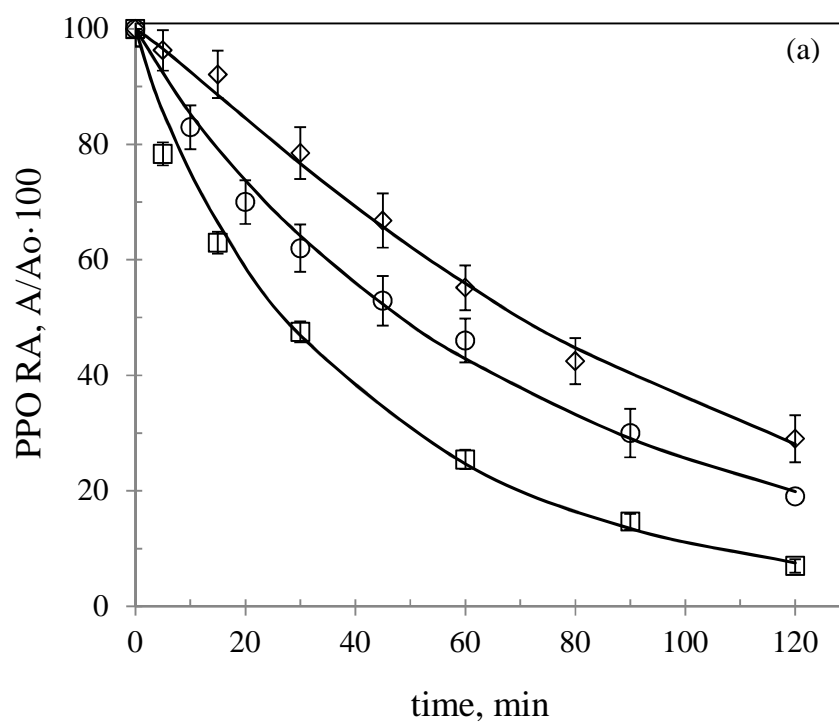
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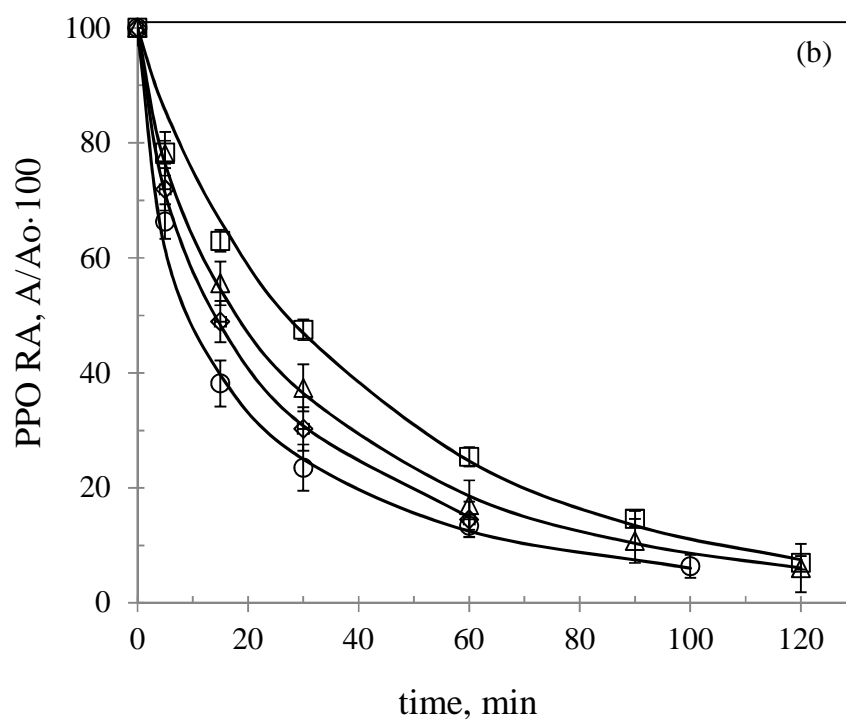
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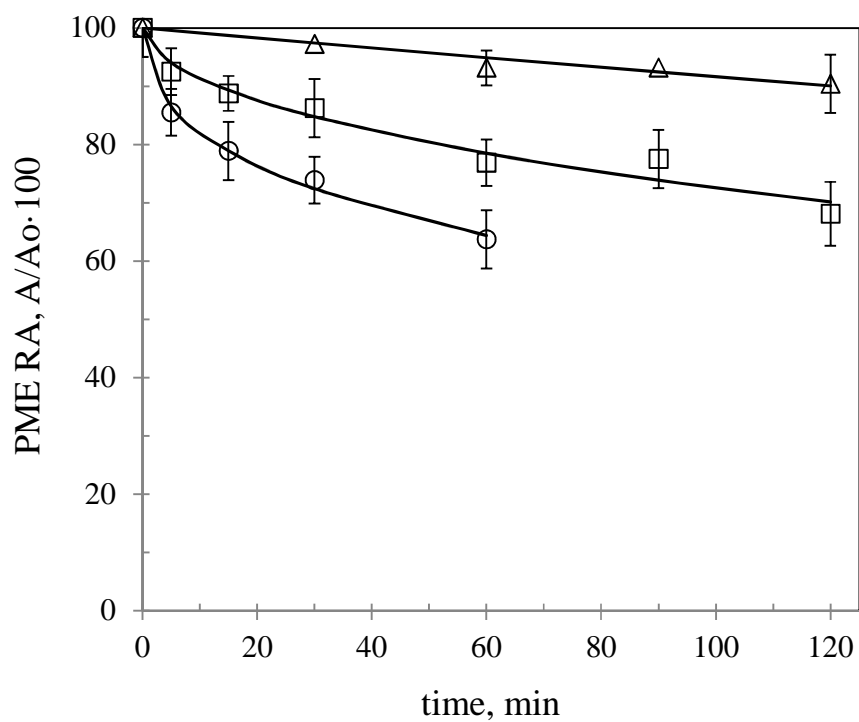


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698 lines represent the Weibull model (Table 2).

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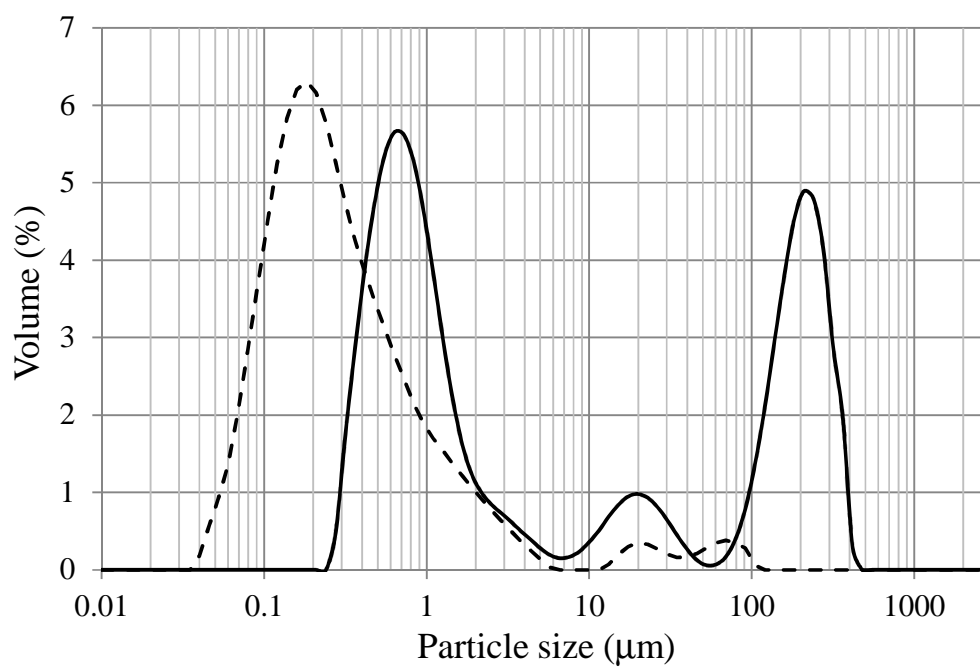
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