

Liquid–Liquid Equilibria for 2-Phenylethan-1-ol + Alkane Systems

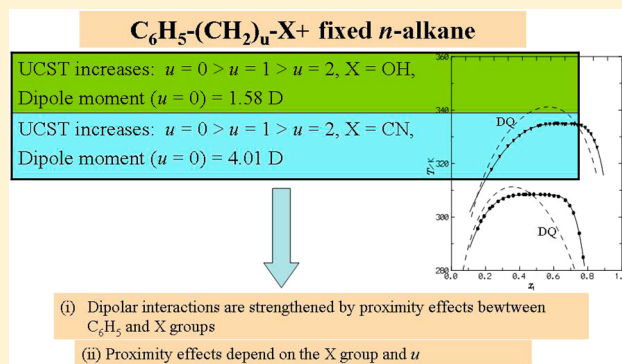
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Supporting Information

ABSTRACT: The liquid–liquid equilibrium (LLE) curves for 2-phenylethan-1-ol (2-phenylethanol, 2PhEtOH) + octane, + decane, + dodecane, + tetradecane or + 2,2,4-trimethylpentane have been determined by a method of turbidimetry using a laser scattering technique. Experimental results reveal that the systems are characterized by an upper critical solution temperature (UCST), which increases linearly with the number of C atoms of the *n*-alkane. In addition, the LLE curves have a rather horizontal top and become skewed to higher mole fractions of the *n*-alkane, when its size increases. For a given *n*-alkane, UCST decreases as follows: phenol > phenylmethanol > 2-PhEtOH, indicating that dipolar interactions decrease in the same sequence. This has been ascribed to a weakening in the same order of the proximity effects between the phenyl and OH groups of the aromatic alkanols. DISQUAC interaction parameters for OH/aliphatic and OH/aromatic contacts in the investigated systems are reported. Phenol, or phenylmethanol or 2-PhEtOH, + *n*-alkane mixtures only differ by the first dispersive Gibbs energy interaction parameter for the (OH/aliphatic) contact.



1. INTRODUCTION

The investigation of liquid mixtures involving aromatic polar compounds is of great interest due to the proximity effects between the aromatic ring (C₆H₅ – group) and the polar X group of the aromatic compound. These effects are intramolecular effects and lead to interactions between the phenyl ring and the X group which are substantially different from those between the mentioned groups when they belong to different molecules.¹ In this framework, we have investigated mixtures including aromatic amines^{2–9} (anilines, 2-amino-1-methylbenzene, 1-phenylmethanamine (benzylamine), 1H-pyrrole, quinoline or imizadoles), aromatic alkanals, ketones, or alkanooates,^{1,10–12} and aromatic nitriles,¹³ 2-phenoxyethanol,¹⁴ or aromatic alkanols (phenol or phenylmethanol).^{15,16} As

continuation, we provide now liquid–liquid (LLE) measurements for binary systems formed by 2-phenylethan-1-ol (2-phenylethanol, 2PhEtOH) and octane, decane, dodecane, tetradecane, or 2,2,4-trimethylpentane. 2-PhEtOH is an aromatic alkanol characterized by its rose-like fragrance and widely used in the cosmetics, perfumery, and food industries.^{17,18} In the pharmaceutical industry, it is also employed due to its antimicrobial properties. Interestingly, 2-PhEtOH is an intermediate in the microbial transformation of L-phenylalanine, an essential amino acid for humans. This makes possible a low cost production of 2-PhEtOH by enzymatic transformation or microbial fermentation through a

natural process where difficult purification problems related to the chemical synthesis are avoided.^{17,19}

2. EXPERIMENTAL SECTION

2.1. Materials. Information on source, purity, water contents, determined by the Karl Fischer method, and density (ρ) of the pure chemicals employed along this investigation is collected in Table 1. All the chemicals were used as received. Density values were obtained from a vibrating-tube densimeter and a sound analyzer, Anton Paar model DSA-5000. The repeatability of the ρ measurements is $5 \times 10^{-3} \text{ kg}\cdot\text{m}^{-3}$, while their relative standard uncertainty is 0.001. Inspection of Table 1 shows that there is a good agreement between our density results and those taken from the literature.

2.2. Apparatus and Procedure. Mixtures were prepared by mass in small Pyrex tubes of the following dimensions: 0.009 m i.d. and about 0.04 m length (free volume of the ampule $\approx 1.17 \times 10^{-6} \text{ m}^3$). The tubes were immediately sealed by capping at 0.1 MPa and 298.15 K. Weights were measured using an analytical balance Sartorius NSU12Sp (weighing accuracy 10^{-8} kg). Mole fractions were calculated on the basis of the relative atomic mass Table of 2015 issued by the

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Table 1. Properties of Pure Compounds at 0.1 MPa and 298.15 K^a

compound	CAS	source	initial mole fraction	$\rho/\text{kg}\cdot\text{m}^{-3\text{a}}$		water content ^b
				exp.	lit.	
2-phenylethanol	60-12-8	Sigma-Aldrich	$\geq 99.9\%\text{c}$	1016.2	1016.1 ⁴⁵	11×10^{-4}
octane	111-65-9	Sigma-Aldrich	$\geq 99\%.4\text{c}$	698.71	698.62 ⁴⁶	35×10^{-4}
decane	124-18-5	Fluka	$\geq 99.8\%\text{c}$	726.35	726.35 ⁴⁶	20×10^{-4}
dodecane	112-40-3	Fluka	$\geq 99.7\%\text{d}$	745.51	745.32 ⁴⁷	25×10^{-4}
tetradecane	629-59-4	Fluka	$\geq 99.5\%\text{c}$	759.27	759.32 ⁴⁴⁷	25×10^{-4}
2,2,4-trimethylpentane	540-84-1	Fluka	$\geq 99.9\%\text{c}$	687.32	687.81 ⁴⁶	28×10^{-4}

^aStandard uncertainties are $u(T) = 0.01 \text{ K}$; $u(P) = 0.5 \text{ kPa}$; the relative standard uncertainty for density is $u_r(\rho) = 0.001$ and 0.02 for water content.

^bIn mass fraction. ^cProvided by the supplier by gas chromatography. ^dBy mass spectrometry.

Table 2. Experimental Liquid–Liquid Equilibrium Temperatures for 2-Phenylethanol (1) + Alkane(2) Mixtures^a at 0.1 MPa

x_1	T/K	x_1	T/K	x_1	T/K	x_1	T/K
2-Phenylethanol (1) + Octane (2)				2-Phenylethanol (1) + Dodecane (2)			
0.1544	295.7	0.4835	308.5	0.5052	325.7	0.8463	314.2
0.1730	298.5	0.5223	308.5	0.5271	325.8	0.8657	310.2
0.1918	300.3	0.5485	308.4	0.5573	325.9	0.8968	303.1
0.2248	303.2	0.5742	308.3	0.5840	325.9		
0.2407	304.0	0.6019	307.9	2-Phenylethanol (1) + Tetradecane (2)			
0.2745	305.9	0.6281	307.7	0.2155	317.8	0.6250	334.8
0.3044	306.9	0.6487	306.9	0.2833	322.7	0.6499	334.9
0.3355	307.7	0.6684	306.3	0.3312	326.6	0.6632	334.7
0.3626	308.1	0.6943	304.3	0.3652	328.7	0.6721	334.8
0.3956	308.4	0.7165	301.6	0.4002	330.5	0.7050	334.9
0.4240	308.5	0.7502	293.9	0.4317	331.9	0.7220	334.7
0.4362	308.5	0.7730	285.0	0.4672	333.1	0.7396	334.4
0.4595	308.5			0.5104	334.0	0.7631	334.2
2-Phenylethanol (1) + Decane (2)				0.5225	334.3	0.7852	333.4
0.1822	303.0	0.5145	317.0	0.5527	334.7	0.8024	332.2
0.2007	305.1	0.54450	317.0	0.5771	334.9	0.8195	331.0
0.2318	308.1	0.5751	316.9	0.6028	334.8	0.8390	328.5
0.2471	309.6	0.5940	316.7	0.6128	335.0	0.8541	326.0
0.2708	311.3	0.6172	316.7	0.6223	335.0		
0.2942	312.8	0.6653	316.0	2-Phenylethanol (1) + 2,2,4-Trimethylpentane (2)			
0.3365	314.7	0.6660	316.2	0.1608	310.3	0.4532	322.4
0.3617	315.3	0.6872	315.6	0.1800	312.9	0.4805	322.5
0.3807	315.7	0.7177	314.4	0.2048	315.6	0.5021	322.4
0.4197	316.6	0.7433	312.6	0.2275	317.3	0.5298	322.2
0.4466	316.6	0.7659	310.2	0.2609	319.0	0.5457	322.3
0.4692	316.8	0.7871	306.7	0.2771	319.8	0.5793	322.1
0.4991	317.0	0.8020	303.8	0.3072	320.8	0.6009	321.6
2-Phenylethanol (1) + Dodecane (2)				0.3137	321.0	0.6317	320.7
0.1908	309.4	0.5996	326.0	0.3361	321.4	0.6464	320.1
0.2483	314.8	0.6247	326.0	0.3512	321.9	0.6742	317.7
0.2676	316.4	0.6405	325.8	0.3771	322.1	0.7534	306.7
0.2923	318.3	0.6733	325.7	0.4044	322.3	0.7742	302.0
0.3352	321.1	0.7062	325.4	0.4214	322.2		
0.3570	322.3	0.7251	325.1	^a Standard uncertainties are $u(x_1) = 0.0030$; $u(p) = 0.5 \text{ kPa}$; the combined expanded uncertainty (0.95 level of confidence) for temperature is $U_c(T) = 0.2 \text{ K}$ in the flat region of the curves and 0.4 K outside this region.			
0.3960	323.7	0.7486	324.2				
0.4303	324.9	0.7728	322.7				
0.4524	325.1	0.7970	320.7				
0.4779	325.4	0.8277	317.5				

70 Commission on Isotopic Abundances and Atomic Weights
71 (IUPAC).²⁰

72 The coexistence curves of liquid–liquid equilibrium were
73 determined by a method of turbidimetry, that is, by means of
74 the observation of the turbidity produced on cooling ($1.2 \text{ K}\cdot$
75 h^{-1}) when a second phase takes place. The process is repeated
76 at least three times. We have previously reported details on the

experimental technique.¹⁴ The equilibrium temperatures were
77 measured using a Pt-1000 resistance. The thermometer was
78 calibrated according to the ITS-90 scale of temperature and the
79 triple point of the water and the fusion point of Ga were
80 considered the fixed points. The precision of the equilibrium
81 temperature measurements is $\pm 0.001 \text{ K}$. The estimated
82 standard uncertainties in the flat region of the coexistence
83

84 curves, and outside of this region are 0.1 and 0.2 K,
85 respectively. The standard uncertainty of the equilibrium mole
86 fraction is 0.0030. This value is determined taking into account
87 that the more volatile component is partially evaporated to the
88 mentioned free volume of the ampule.

3. EXPERIMENTAL RESULTS

89 Experimental results determined in this work, the directly
90 measured liquid–liquid equilibrium temperatures, T , versus x_1 ,
91 the mole fraction of 2-PhEtOH, for the systems with n -C₈, n -
92 C₁₀, n -C₁₂, n -C₁₄, or 2,2,4-trimethylpentane, are collected in
93 Table 2 (Figure 1). As in many systems previously

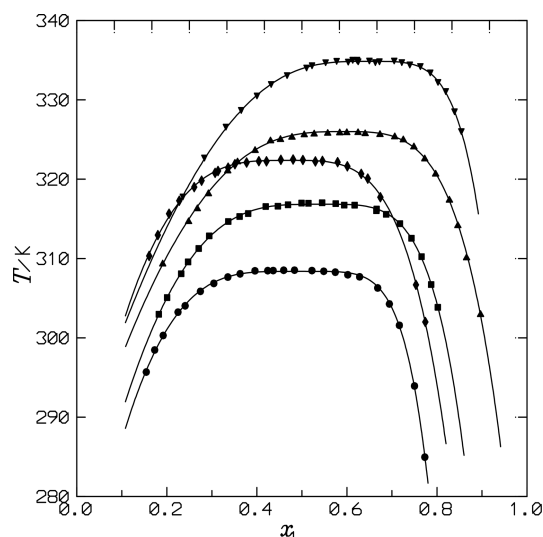


Figure 1. LLE for 2-phenylethanol(1) + octane(2) (●); + decane(2) (■); + dodecane(2) (▲); + tetradecane(2) (▼), or +2,2,4-trimethylpentane (◆) systems. Points, experimental results (this work); solid lines, calculations using the parameters listed in Table 3.

94 investigated,^{1,3–5,9,11–16} the LLE curves of the present mixtures
95 are characterized by some typical features: (i) they show a
96 rather flat maximum (Figure 1); (ii) the curves become
97 progressively skewed toward higher x_1 values when the chain
98 length of the alkane is increased (Figure 1); (iii) the upper
99 critical solution temperature, UCST increases with the number
100 of C atoms of the n -alkane (Table 3).

101 The experimental (x_1, T) data of each system were correlated
102 by means of the equation^{21,22}

$$T/K = T_c/K + k|y - y_c|^m \quad (1) \quad 103$$

where 104

$$y = \frac{\alpha x_1}{1 + x_1(\alpha - 1)} \quad (2) \quad 105$$

$$y_c = \frac{\alpha x_{1c}}{1 + x_{1c}(\alpha - 1)} \quad (3) \quad 106$$

In these equations, m , k , α , T_c , and x_{1c} stand for the parameters
107 which must be adjusted against the experimental data. The
108 coordinates of the critical point are denoted by (x_{1c}, T_c). It is
109 remarkable that when $\alpha = 1$, eq 1 is similar to^{23–25}
110

$$\Delta\lambda = B\tau^\beta \quad (4) \quad 111$$

In eq 4, $\Delta\lambda_1 = \lambda_1' - \lambda_2''$ is any order parameter, that is, any
112 density variable in the conjugate phase. Particularly, in this
113 research, $\lambda_1 = x_1$. In addition, $\tau = (T_c - T)/T_c$ is the reduced
114 temperature and β is the critical exponent related to $\Delta\lambda_1$. It
115 is well-known that the critical exponent β depends on the theory
116 applied to its determination.^{23,26}
117

The m , k , α , T_c , and x_{1c} parameters were determined through
118 an adjustment based on a Marquardt algorithm²⁷ with all the
119 points weighted equally. Final values of m , k , α , T_c , and x_{1c}
120 and of the standard deviations for LLE temperatures, $\sigma(T)$, are
121 given in Table 3. The $\sigma(T)$ values are calculated from
122

$$(\sigma(T)/K) = \left[\sum (T_{\text{exp}}/K - T_{\text{calc}}/K)^2 / (N - n) \right]^{1/2} \quad (5) \quad 123$$

Here, N denotes the number of data points, and n ($= 5$)
124 denotes the number of adjusted parameters. Results listed in
125 Table 3 show that eq 1 fits well the experimental measure-
126 ments.
127

The UCST for the 2,2,4-trimethylpentane system is available
128 in the literature.²⁸ The value, 322.15 K, is in rather good
129 agreement with our result (322.9 K, Table 3). A part of the
130 observed difference may be due to the use of the method of
131 equal volumes and solvent applied in the determination of the
132 literature value of UCST, where, in addition, no information is
133 provided about the rate of temperature change.
134

4. DISCUSSION

Below we are reporting values of excess molar enthalpies, H_m^E ,
135 at equimolar composition and 298.15 K. Moreover, we consider
136 aromatic polar compounds of the type: C₆H₅ – (CH₂)_{*n*} – X (X
137

Table 3. Coefficients in Equation 1 for the Fitting of the (x_1, T) Pairs Listed in Table 2 for 2-Phenylethanol (1) + Alkane(2) Mixtures; $\sigma(T)$ is the Standard Deviation Defined by Equation 5

N^a	m	k	α	T_c/K	x_{1c}	$\sigma(T)/K$
24	4.471	– 5265	2-Phenylethanol(1) + Octane(2)			
			0.533	308.4 (311.3) ^b	0.499 (0.343) ^b	0.16
26	3.761	– 1322	2-phenylethanol(1) + Decane(2)			
			0.597	316.8 (317.3) ^b	0.543 (0.431) ^b	0.13
27	3.218	– 543	2-Phenylethanol(1) + Dodecane(2)			
			0.586	326.0 (330.4) ^b	0.593 (0.506) ^b	0.17
27	3.583	– 952	2-Phenylethanol(1) + Tetradecane(2)			
			0.419	334.8 (341.2) ^b	0.651 (0.573) ^b	0.11
25	3.571	– 1200	0.743	322.4	0.471	0.18

^aNumber of experimental data points. ^bDISQUAC value obtained using interchange coefficients listed in Table 4.

138 = OH, NH₂, CN, NO₂, CHO), or C₆H₅ - (CH₂)_u - X - CH₃,
 139 (X = CO, OCO) with different *u* values.

140 First, we remark the very different behavior of mixtures
 141 formed by 1-alkanol or aromatic alkanol and one *n*-alkane.
 142 Systems involving 1-alkanols are characterized by rather low H_m^E
 143 values. Thus, H_m^E (*n*-C₇)/J·mol⁻¹ = 487 (heptan-1-ol);²⁹ 462
 144 (octan-1-ol).³⁰ In addition, the H_m^E curves are skewed toward
 145 low alcohol concentrations.^{29–31} These features have been
 146 explained in terms of the alcohol self-association, which is
 147 scarcely broken by alkanes. In contrast, mixtures containing
 148 aromatic alkanols show LLE curves, with moderately high
 149 UCST values (Figures 2–4). This clearly reveals that the dipolar

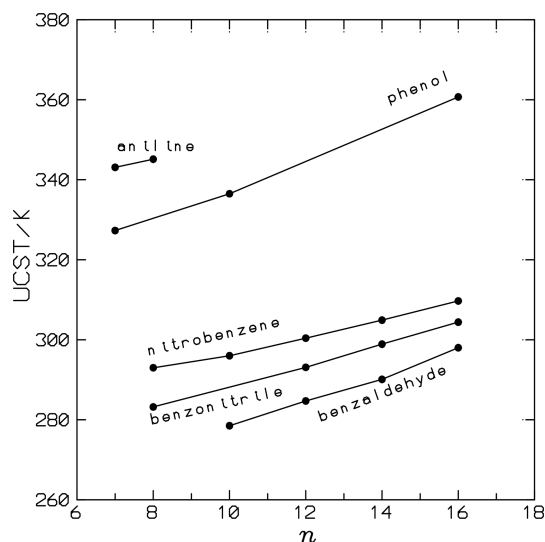


Figure 2. Upper critical solution temperatures, UCST for C₆H₅ - X(1) + *n*-alkane(2) systems (X = OH, NH₂, CN, NO₂, CHO), versus *n*, the number of C atoms in the alkane. Lines are only for the aid of the eye. For experimental data, see aniline,^{34,48} phenol,^{35,49,50} nitrobenzene,^{51–55} benzonitrile,^{36,56–58} and benzaldehyde.¹¹

150 interactions between alkanol molecules are strengthened by the
 151 presence of the C₆H₅- and -OH groups in the same molecule.
 152 Interestingly, the replacement of the *n*-alkane by an aromatic
 153 compound, say benzene, in mixtures with a given 1-alkanol
 154 leads to increased H_m^E values. For example; H_m^E (benzene)/J·
 155 mol⁻¹ = 1109 (hexan-1-ol);³² 1130 (octan-1-ol).³³ That is,
 156 aromatic compounds are more active molecules than *n*-alkanes
 157 when breaking the alcohol network. In summary, intermolec-
 158 ular effects between the -OH and aromatic groups increase H_m^E
 159 values compared to those of 1-alkanol + *n*-alkane systems, while
 160 intramolecular effects between the mentioned groups lead to
 161 solutions become more immiscible.

162 The strength of the intramolecular effects between the
 163 C₆H₅- and the X groups depends on the polar group
 164 considered. Figure 2 shows that UCST/K values of mixtures
 165 formed by an *n*-alkane and an aromatic polar component with *u*
 166 = 0 change in the order: 343.1 (aniline + heptane)³⁴ > 327.3
 167 (phenol + heptane)³⁵ > 283.2 (benzonitrile + octane)³⁶ > 278.5
 168 (benzaldehyde + decane).¹¹ In contrast, the corresponding μ/D
 169 values change in the sequence: 4.01 (benzonitrile) > 3
 170 (benzaldehyde) > 1.58 (phenol) \approx (1.57) aniline (Table S1,
 171 Supporting Information).³⁷ The observed variation of UCST
 172 with μ reveals that dipolar interactions are not merely related to
 173 the μ value of the polar compound, but they are also closely
 174 related to the proximity effects, which are stronger in solutions

with phenol or aniline. In addition, self-association effects seem
 175 to be not very important as the UCST values of systems with
 176 the less self-associated aniline are higher than those of phenol
 177 mixtures (Figure 2). Nevertheless, the behavior described above
 178 may be different when the involved polar compound is
 179 characterized by *u* \neq 0, depending on the specific group.
 180 This is shown in Figures 3 and 4, where one can see that UCST
 181 184

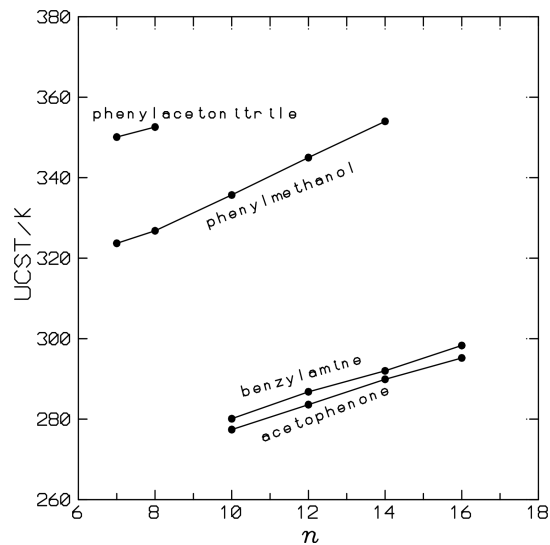


Figure 3. Upper critical solution temperatures, UCST for C₆H₅ - CH₂ - X(1), or C₆H₅ - CH₂ - X - CH₃ + *n*-alkane(2) systems (X = OH, NH₂, CN, CO), versus *n*, the number of C atoms in the alkane. Lines are only for the aid of the eye. For experimental data, see phenylacetone nitrile,¹³ phenylmethanol,¹⁶ benzylamine,⁵ and acetophenone.¹⁰

values of solutions containing aromatic nitriles, rather polar
 182 compounds (Table Table S1, Supporting Information), are 183

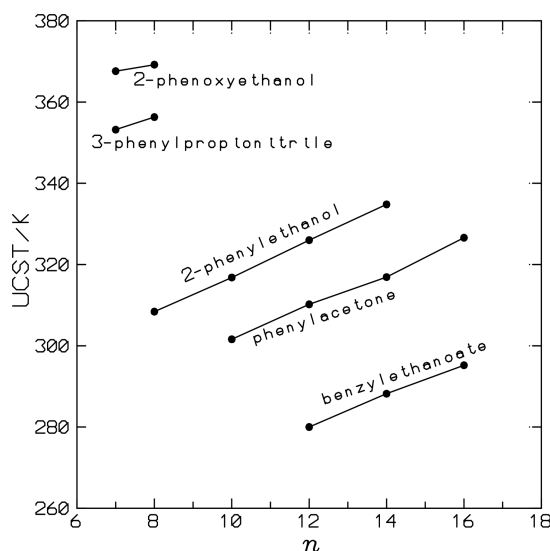


Figure 4. Upper critical solution temperatures, UCST for C₆H₅ - (CH₂)₂ - X(1), or C₆H₅ - (CH₂)₂ - X - CH₃(1), or 2-phenoxyethanol(1) + *n*-alkane(2) systems (X = OH, CN, CO, OCO), versus *n*, the number of C atoms in the alkane. Lines are only for the aid of the eye. For experimental data, see 3-phenylpropan nitrile,¹³ 2-phenylethanol (this work), 1-phenylpropan-2-one (phenylacetone),¹ benzylethanoate,^{1,12} 2-phenoxyethanol.¹⁴

Table 4. Dispersive (DIS) and Quasichemical (QUAC) Interchange Coefficients, $C_{st,l}^{\text{DIS}}$ and $C_{st,l}^{\text{QUAC}}$, for (s,t) Contacts in (2-PhEtOH + *n*-Alkane) Mixtures (*l* = 1, Gibbs Energy; *l* = 2, Enthalpy; *l* = 3, Heat Capacity)

contact ^a (s,t)	CH ₃ (CH ₂) _{<i>n</i>} CH ₃	$C_{st,1}^{\text{DIS}}$	$C_{st,2}^{\text{DIS}}$	$C_{st,3}^{\text{DIS}}$	$C_{st,1}^{\text{QUAC}}$	$C_{st,2}^{\text{QUAC}}$	$C_{st,3}^{\text{QUAC}}$
(b,h)		4.80	− 2.65		5.70	13	
(a,h)	<i>n</i> ≤ 7	3.55	0.50	− 5	11.25	16	12
(a,h)	<i>n</i> = 8	3.36	0.50	− 5	11.25	16	12
(a,h)	<i>n</i> > 8	3.36	0.50	5	11.25	16	30

^aType a, aliphatic in alkane, or 2-PhEtOH; type b, C₆H₅ in 2-PhEtOH; type h, OH, in 2-PhEtOH

184 higher than those of systems with aromatic alkanols or
185 alkanones, benzylamine, or benzylethanoate. Therefore, the
186 variation of UCSTs with *u* for mixtures with a fixed alkane also
187 depends on the group. Thus, UCST/K changes in the order:
188 327.3 (phenol (*u* = 0) + heptane)³⁵ > 323.7 (phenylmethanol
189 (*u* = 1) + heptane)¹⁶ > 308.4 (2-phenylethanol (*u* = 2) +
190 octane) (this work), while UCST(octane)/K = 356.3 (3-
191 phenylpropionitrile (*u* = 2))¹³ > 352.6 (phenylacetonitrile (*u* =
192 1))¹³ > 283.2 (benzonitrile (*u* = 0)).³⁶

193 On the other hand, the replacement of octane by 2,2,4-
194 trimethylpentane in systems with 2-PhEtOH leads to increased
195 UCST values. This trend is also held for mixtures involving
196 other aromatic polar compounds (phenol, nitriles, alkanones, or
197 aniline).¹³ Different results can be obtained depending on the
198 nature of the solute and of the branching of the alkane, as we
199 have shown from a detailed investigation on tertiary amide +
200 alkane mixtures.³⁸

201 It is pertinent to compare UCST values for mixtures with 2-
202 PhEtOH or 2-phenoxyethanol (Figure 4). The latter have
203 higher critical temperatures, which can be ascribed to such
204 systems are also characterized by proximity effects between the
205 O and OH groups.³⁹ Mixtures involving linear alkoxyethanols
206 also show higher UCST values than the corresponding mixtures
207 with homomorphic 1-alkanols. For example, for the 2-
208 methoxyethanol + heptane system, UCST = 319.7 K,⁴⁰ while
209 $H_m^E/\text{J}\cdot\text{mol}^{-1}$ of the mixture penta-1-ol (isomeric alkanol of 2-
210 methoxyethanol) + heptane is 575.⁴¹

211 Finally, we have applied the DISQUAC group contribution
212 model^{42,43} to represent the LLE curves of the 2-PhEtOH + *n*-
213 alkane systems (Figure 1, Supporting Information). The main
214 features of the model can be found elsewhere.^{42,43} Here, we
215 merely remark on the following: (i) The geometrical
216 parameters of the groups referred in the work, C₆H₅, aliphatic,
217 and OH, are available in the literature.¹⁵ (ii) The temperature
218 dependence of the interaction parameters is described by
219 means of DIS (dispersive) and QUAC (quasichemical)
220 interchange coefficients,^{42,43} $C_{st,l}^{\text{DIS}}$; $C_{st,l}^{\text{QUAC}}$ where *s* ≠ *t* are two
221 contact surfaces present in the mixture and *l* = 1 (Gibbs
222 energy); *l* = 2 (enthalpy); *l* = 3 (heat capacity). (iii) 2-PhEtOH
223 + *n*-alkane mixtures are built by the following surfaces: type a,
224 aliphatic (CH₃, CH₂, in *n*-alkanes, or 2-PhEtOH); type b,
225 aromatic (C₆H₅ in 2-PhEtOH), and type h, hydroxyl (OH in 2-
226 PhEtOH). These surfaces generate three contacts: (a,b); (a,h),
227 and (b,h). The (a,b) contact is characterized by purely
228 dispersive interaction parameters, previously determined from
229 the study of alkyl-benzene + alkane mixtures.⁴⁴ In contrast,
230 interactions parameters for the (a,h) and (b,h) contacts are
231 represented by both DIS and QUAC interchange coefficients.
232 (iv) In our work on phenylmethanol + *n*-alkane systems,¹⁶ we
233 showed that the corresponding coordinates of the critical points
234 can be fairly well described using the values of $C_{bh,l}^{\text{DIS}}$, $C_{sh,l}^{\text{DIS}}$ (*s* = a,
235 b; *l* = 2, 3), and $C_{sh,l}^{\text{QUAC}}$ (*s* = a, b and *l* = 1, 2, 3) of the phenol
236 mixtures, and merely fitting the coefficient $C_{ah,1}^{\text{DIS}}$. Here, we have

237 applied the same approach. The final interaction parameters are
238 listed in Table 4. DISQUAC results obtained for (*x*_{1c}, *T*_c) are
239 listed in Table 3. The coordinates of the critical points are
240 described in the correct range of composition and temperature,
241 although our theoretical LLE curves are more rounded than the
242 experimental ones (Figure S1, Supporting Information). This
243 can be explained taking into account that DISQUAC
244 calculations are conducted assuming erroneously that the
245 excess functions are analytical in the vicinity of the critical
246 points, although really, at the mentioned condition, thermody-
247 namic properties follow scaling laws with universal critical
248 exponents and universal scaling functions.²³ More details on
249 this regard can be found elsewhere.¹⁶ We conclude remarking
250 that our DISQUAC results suggest that systems including an
251 aromatic alkanol of the type C₆H₅ − (CH₂)_{*u*} − OH (*u* = 0, 1,
252 2) can be characterized by the same QUAC interaction
253 parameters for the OH/aliphatic and OH/aromatic contacts,
254 and form an homologous series. The mixtures aniline² or 2-
255 methylaniline⁵ + alkane behave similarly.

5. CONCLUSIONS

256 Liquid–liquid equilibrium temperatures versus composition
257 have been experimentally determined for 2-PhEtOH + octane,
258 + decane, + dodecane, + tetradecane, or + 2,2,4-trimethylpen-
259 tane systems. All the curves show a UCST, which increases
260 linearly with the alkane size. Proximity effects become weaker
261 in the sequence: phenol > phenylmethanol > 2-PhEtOH.
262 DISQUAC interaction parameters are reported for 2-PhEtOH
263 + *n*-alkane systems. Mixtures with phenol, phenylmethanol, or
264 2-phenylethanol are characterized by the same $C_{sh,l}^{\text{QUAC}}$ (*s* = a, b; *l* =
265 1, 2, 3) and $C_{sh,l}^{\text{DIS}}$ (*s* = a, b; *l* = 2, 3) coefficients, while differ
266 only by the $C_{ah,1}^{\text{DIS}}$ coefficients.

■ ASSOCIATED CONTENT

📄 Supporting Information

267 The Supporting Information is available free of charge on the
268 ACS Publications website at DOI: 10.1021/acs.jced.7b00869.

269 Table S1 lists dipole moments of aromatic polar
270 compounds considered along the work; Figure S1
271 shows a comparison between experimental results and
272 DISQUAC calculations (PDF)

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